## Master Training Program on Water (Water Supply, In-house Processing, End-of-Pipe) in Textile and Garment factories

Promotion of Sustainability in the Textile and Garment Industry in Asia - FABRIC







Day 6: Presentation 2

## Making Treated effluent fit for recovery systems



Contents

Objectives of advanced treatment

Membrane bio-reactor

Filters for polishing treated effluent

Chemical oxidation for organic removal from treated effluent

### Need for advanced treatment before effluent recovery



- Most effluent recovery systems use membranes for purification
- Most membranes are designed to treat saline, but otherwise pure water, as input
- Membranes are prone to fouling (plugging) if treated effluent high in
  - Fine suspended solids (silt)
  - Organic compounds (BOD/COD)
  - Microbial population (mostly bacteria)
  - High hardness
- Make treated effluent fit for membrane systems such as Reverse Osmosis is a major challenge.
- Advanced tertiary treatment systems are useful for this purpose.

#### Basic concept and overview of advanced treatment

- Final treatment stage, to comply with norms and make effluent fit for recycle systems such as Reverse Osmosis.
- Single stage or using combination of tertiary systems.
- Focus on
  - ✓ Reduction of color
  - ✓ Reduction of turbidity and suspended solids
  - ✓ Destruction of pathogens
  - ✓ Removal of residual organics
  - ✓ sometimes for aesthetic purpose and as precautionary or complimentary measure

### Basic concept and overview of tertiary treatment



#### **Common tertiary treatment systems**

- **Disinfection** mainly to kill micro-organisms in treated effluent and some for organic removal.
- Filters, using filter media to filter out suspended particles in effluent
- Adsorption filters most commonly activated carbon filters to remove organics
- Oxidation systems to oxidize residual organics in treated effluent

### Basic concept and overview of tertiary treatment



#### Other tertiary treatment systems

- Chemical precipitation systems for removal of phosphates/metals.
- Softening using lime/soda softening or zeolite softeners
- Membrane based filtrations (using ultra filters or nanofilters) – membrane bio-reactor incorporates ultra filtration in itself.

## Advanced treatment systems

#### Advanced wastewater treatment

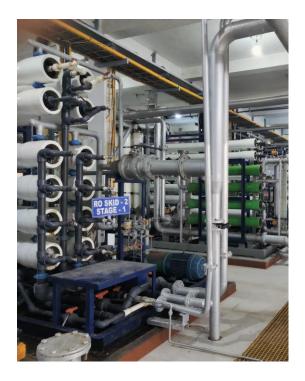
- To overcome the limitations of conventional biological treatment & make it for membranes, improved biological systems developed.
- Recently, many advanced biological treatment systems are being used for textile effluent treatment.
- It comprises of modification of conventional treatment systems such as MBBR/FAB as well as in-situ units such SBR or RBC type units.
- While these systems consumes relatively lesser space and provide better treatment, it does not effectively address issues such as space constraints, pre-treatment requirement for recycling, sludge generation etc.
- Membrane bio-reactor (MBR) is being increasingly considered as an effective biological alternative for this purpose.



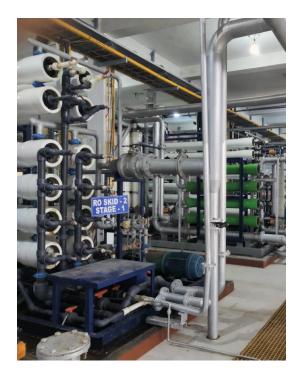
### Membrane bio-reactor as a solution



- Membrane bio-reactor is a modified biological treatment which use a membrane filter for solids separation.
- Membranes are fine filters can filter out all suspended and colloidal solids, some times even dissolved solids.
- Membrane bio-reactor consumes much less space and produces effluent with clarity & no suspended solids.
- Due to its high solids retention, it can treat recalcitrant organics much better.
- It does not have much of the operational issues in secondary clarification such as sludge sludge bulking.
- It also produces relatively less sludge and need much lesser pre-treatment for ZLD.

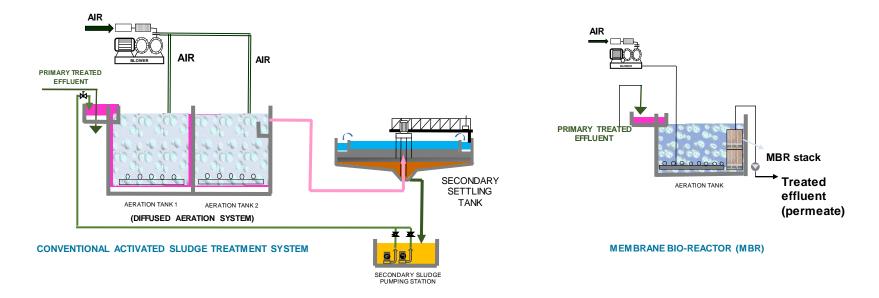


- MBR is basically an activated sludge treatment, except instead of a secondary settling tank to separate bio-solids, a micro or ultra filtration is used.
- No limitation due to settling characteristics of MLSS. So, much higher MLSS in aeration tank. Hence size of aeration and area needed for ETP comes down.
- MBR concept developed in the late 1960's, but was not popular due to high power consumption till end of 80's. Then submerged MBR was developed.



- Submerged MBR use less power. But frequent membranes fouling an issue.
- The external MBR, generally called side stream MBR, continued to be the preferred MBR system for small plants.
- Generally MBR is preferred over conventional system where the space availability is a concern and recycle options are considered for future.

#### **Conventional activated sludge system Vs MBR**



In conventional activated sludge treatment system, we have aeration tank with aeration, followed by secondary clarifier and sludge return. In MBR ,the clear effluent is sucked out through an ultrafiltration.

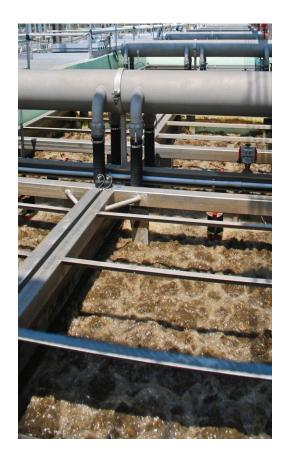


- MBR has basically two components: aeration tank and set of micro/ultra filter.
- In submerged MBR, membranes, tacked in cassettes, is installed in aeration tank.
- The filtrate is sucked out using vacuum/ pressure pump, leaving MLSS in the tank
- In side stream MBR, aeration tank contents is pumped into an external MBR mounted on a skid.
- The filtered clear effluent is discharged. Retained MLSS solution is sent back to aeration tank.
- A modification of side-stream MBR is called air-lift scouring by air for additional backwash.



#### Performance of MBR Vs conventional treatment

- MBR effluent may have zero suspended solids. The treated effluent turbid is generally less than 10 NTU.
- Since only dissolved organics escape the system, the BOD/COD reduction could be 40-60% better than conventional
- The mean cell retention time in MBR can be 80-120 days as against the 25-30 days in conventional. This ensures better reduction of recalcitrant/refractory organics.
- Overall space requirement of MBR based ETP can be about 60% of the conventional ETP.
- The sludge production from the unit can be 30-45% less than conventional treatment.



#### **Operating conditions of MBR**

- MLSS levels in MBR would be much higher than conventional activated sludge system. The typical range is 10000-15000 mg/l.
- Submerged MBR can also be in two ways:
  - where the membrane cassettes are installed directly in the aeration tank
  - aeration tank is constructed in two compartments and membrane stack is installed in one compartment.
- Submerged MBR normally consumes power @ 0.5 kWh/m<sup>3</sup> of effluent treated Vs side stream @ 2-4 kWh/m3 depending on the type of effluent.



#### **Operating conditions of MBR**

- Because the solids are filtered & retained in the aeration tank, sludge retention time in an MBR is high.
- Typical SRT is 30-50 days. Higher SRT is possible, but increases fouling.
- Fouling of membrane by MLSS particles, colloids etc. is the major concern of MBR.
- Once fouling increases, the flow drops. Once membrane is cleaned, the flow rate (often called flux) through the membrane increases.

- Better removal of BOD/COD and pathogens .
- With no suspended solids, clear & less turbid treated effluent.
- Lesser pre-treatment when effluent recovery is considered.
- Much less area compared to conventional ASP.

#### MBR Advantages

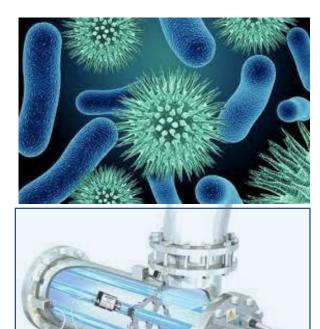


- Higher capital cost
- Higher O & M cost additional power and membrane cleaning/replacement.
- System is more sensitive and complex in operation.
- Membrane replacement add to the list of consumables.
- Improper solids control results membrane clogging.

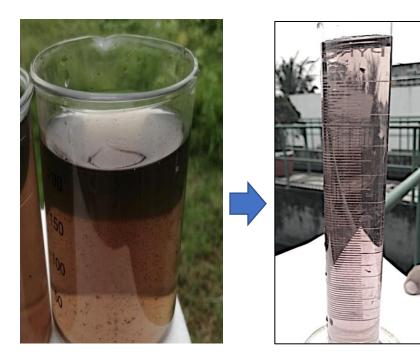
MBR disadvantages

# Tertiary treatment systems - Disinfection

### **Tertiary treatment systems - Disinfection**



- To kill micro-organisms, specifically pathogens in treated effluent
- Chlorination **most common** disinfection system mixing effluent with chlorine gas in contact chambers or dosage of hypo-chlorites.
- Increased efficiency of chlorination with higher dosage, lower pH, higher temperature and longer contact time
- UV radiation can kill pathogen: effluent passing through chamber illuminated by UV rays from UV lamp
- Different types UV-A, UV-B, UV-C : the last more effective & consume more power.



#### **Filtration**

- Used for removal of suspended solids in treated effluent
  - Also partly reducing BOD/COD by removing some organics (like MLSS particle) in the suspended solids
- Done by gravity or pressure filters
  - Slow sand filters using gravity (only small ETPs)
  - Pressure sand filters using vessel filled with filter media with effluent being pumped and filter under pressure
  - Fine filtrations (such as pre-treatment of membrane) with cartridge filters



#### **Filtration – Pressure filters**

- Common types in wastewater treatment:
  - ✓ Pressure sand filters
  - ✓ Multi-grade filters
  - ✓ Dual media filters
- Similar in construction and operational pattern but varying in composition of filter media
- made of FRP, MS (often rubber lined) and stainless steel
- New types of media coming to market every year.



#### **Filtration – Pressure filters**

- Measurement of **operational efficiency** through parameters like **filtration rate, head loss and frequency of backwashing** needed.
- Backwashing whenever pressure drop more than 1 bar.
- Sometimes preceded by air scouring for agitating media with scrubbing action and loosens retained solids.
- Common filtration media
  - ✓ most common silica sand and anthracite coal
  - ✓ quartz sand, garnet, magnetite
- Size and shape of filter media affecting efficiency
  - ✓ Smooth and rounded better than sharp and angular media
  - ✓ Most suspended solids at surface (top 5 10 cms), gradually solids percolating down to prevent rapid pressure drop

### Pressure filters: Operation cycle

#### Service

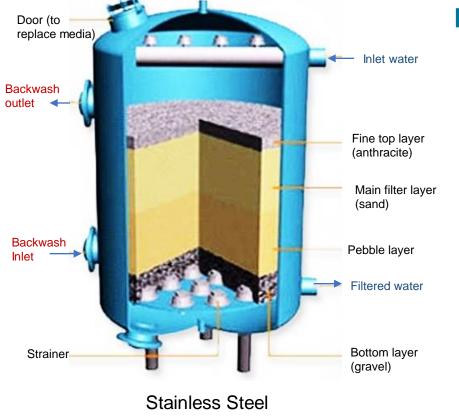
- Inlet water is pumped down through the media via the distribution tube.
- Collect the drained water as filtered water.

#### Backwash

- Flow is reversed.
- The flow is forced through the bottom and up through the media.
- Backwash lifts media and causes scouring
- Collected dust and debris is flushed to the drain

#### **Slow Rinse**

- Use clean water allowed to flow down through media bed & distribution tube to drain.
- With autovalves and controls, entire backwash & rise can be programmed based on fixed quantity of flow, at scheduled time or based on differential pressure.



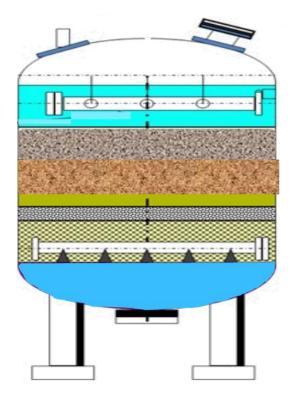
#### **Filtration: Pressure sand filters**

- Usually cylindrical vessel filled with filter media.
- Vertical or horizontal orientation
- Set of frontal pipe work and valves
- Graded silica quartz sand
- Sand layer supported by under-bed of pebble/gravel.
- Water admitted via top distributor
- Under-drain collecting filtered water



#### **Filtration : Multigrade filters**

- similar to pressure sand filter in construction with cylindrical vessel and identical piping/valves
- Same way of operation and backwashing
- coarse and fine media mixed together in fixed proportion.
- filtration efficiency not as fine as in pressure sand filter but turbidity reduction better
- Higher flow rate and turbidity reduction than pressure sand filter
- Less filtration efficiency, more energy and higher backwash than pressure sand filters.



#### Filtration – Dual media filters

- similar to pressure sand filter in construction with cylindrical vessel and identical piping/valves
- Same way of operation and backwashing
- sand-anthracite filter or multi-media used for removal of turbidity and suspended solids
- Remove TSS as low as 10 20 microns
- higher filtration rate & flow than other pressure filters.
- Backwash water need & frequency of backwash higher and media has lower life.



#### **Filtration – Cartridge filters**

- used for very fine filtration e.g. pre-treatment of membranes
- cartridge filters considered as consumables
  - $\checkmark$  possible to clean by soaking in cleaning solution
  - $\checkmark$  to be replaced once clogged irreversibly
- usually very small in construction
- generally used in-line of pumping lines
- usually pore sizes in range of 0.2 20 microns
  - ✓ smaller pore size = shorter replacement period
- There are surface filters & depth filters

## Tertiary treatment systems – Removal of organics

+C-CT2N

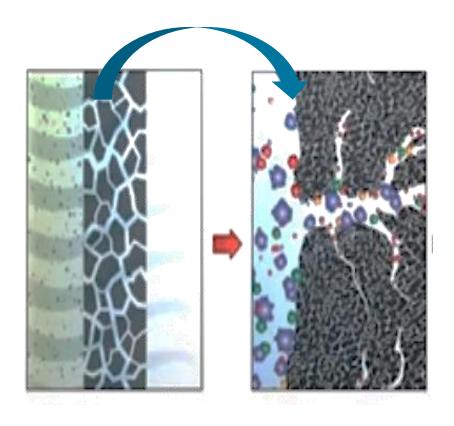
Image: Center Enamel

#### Basic concept and overview of tertiary treatment

#### **Options for management of residual organics**

- Treated effluent containing organics not removed in biological treatment since on bio-degradable to lesser extent
- Tertiary treatment systems for removal of residual organics:
  - Adsorption of organics in adsorbent media, such as activated carbon filters and organic scavengers.
  - Advanced oxidation systems
  - ✓ Ozonation of treated effluent
  - ✓ Fenton treatment: Oxidation catalyzed by iron

### Tertiary treatment systems - Adsorption



#### **Activated carbon filtration**

# Adsorption = adhesion of ions or molecules to surface

- In effluent treatment entrapment of organics (or other contaminants like chlorine) in adsorbent medium
- Physical entrapment in voids of porous medium or attachment to surface due to surface charge
- Activated carbon: Inert solid adsorbent material made from almost any carbon containing feedstock (e.g. wood, coconut shells and coal)
- Porous, inexpensive and high surface area per gram

### Tertiary treatment systems - Adsorption



#### **Activated carbon filters**

- similar in construction to pressure sand filters
- activated carbon as filter media
- commonly granulated activated carbon with 0.4 1 mm diameter or powdered activated carbon
- backwash process similar to pressure sand filters but without air scouring
- strainers at bottom to prevent carbon from flowing out with filtered and at top to prevent loss of carbon during backwash
- carbon media to be replaced once exhausted
- regeneration presently not economical

#### Tertiary treatment systems – Advanced oxidation

Advanced oxidation processes = chemical treatment process for removing organic (and sometimes inorganic) pollutants

- Common systems
  - ✓ Ozone
  - ✓ **Hydrogen peroxide** with or without UV radiation
  - ✓ Fenton treatment
- Concept
  - $\checkmark$  Hydroxyl radical (OH-) and nascent oxygen as active reactants
  - ✓ Hydroxyl radicals produced in water with primary oxidants like oxygen, ozone and peroxides enhanced with energy sources or catalysts

### Tertiary treatment systems – Advanced oxidation



AOP system by NOVEXX

#### **Photochemical oxidation process**

- Hydroxyl radicals present in chemicals with extra oxygen atoms
  - ✓ generation enhanced by radiation with UV rays
    ➢ H2O2 + UV → 2·OH
- Organics pollutants oxidized by hydroxyl radical and broken into simpler organics and further oxidized into carbon dioxide
  - ✓ **Higher efficiency in acidic condit**ions (optimal pH 3 6)
  - Natural organic matter or carbonate species reducing effectiveness
  - ✓ Reduced metal ions (e.g. Ferrous and Manganous) reducing effectiveness since consuming excess oxygen

### Advanced oxidation

- Low space requirement
- Complete degradation of organics
- Fast reaction and very lower retention times vis-à-vis others
- Treatment of wide range of organics
- Complete disinfection too
- No sludge production

Advanced oxidation Advantages



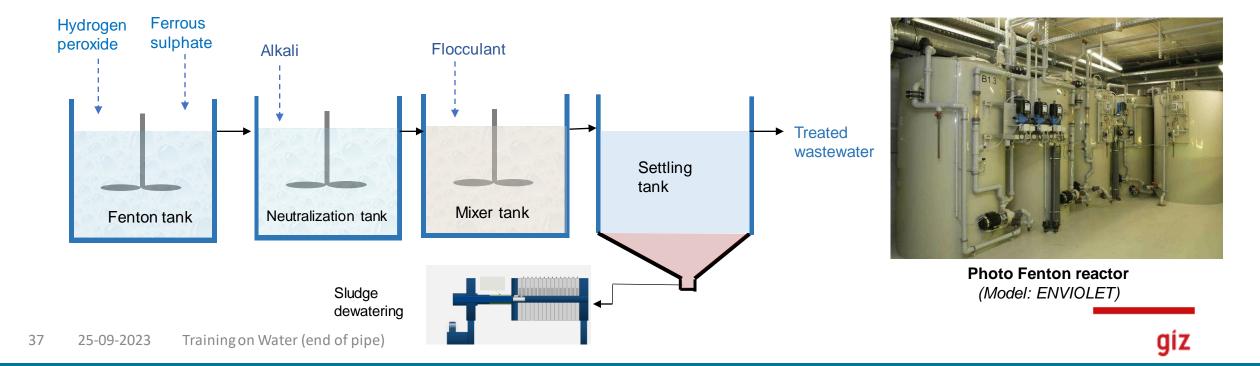
- Need for highly skilled labor to operate and control
- High capital and operating & maintenance costs
- Complex chemistry
- Need to control and remove of product of oxidation.
- Residuals affecting membranes if proper anti-oxidant control not ensured

Advanced oxidation disadvantages

#### Tertiary treatment systems – Advanced oxidation

#### Fenton treatment

- Popular variant type of advanced oxidation (also as further advanced photo Fenton system.
- Based on liberation of OH radicals from H<sub>2</sub>O<sub>2</sub> catalyzed by ferrous ions (in photo Fenton with use of UV radiation)
- Oxides of iron produced in reaction catalyzing oxidation of organics by OH radicals



### Fenton Treatment

- Relatively lower capital cost
- Simple and easy process
- Suitable for all organic materials and some heavy metals
- No concentration of contaminants like salts

- Generation of ferric sludge for dewatering/disposal
- High operation and maintenance costs: peroxide and pH management
- Need to adhere to strict pH range

Fenton system Advantages



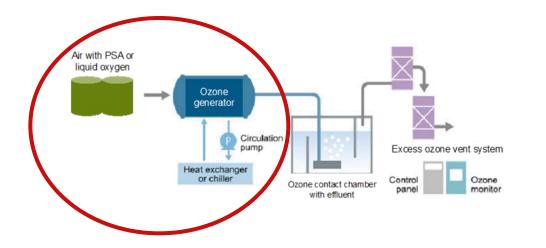
Fenton system disadvantages

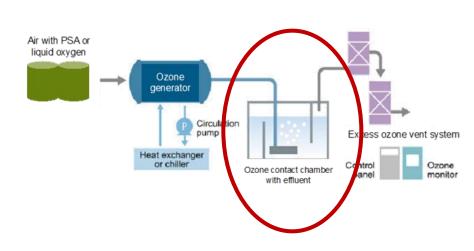
#### **Basic concept**

- Ozone (O3) = oxygen gas with additional oxygen atom
  - pale blue gas with distinctively pungent smell and potentially toxic
- Ozone generated in most ETPs from oxygen-bearing gas subjected to electric field or UV
  - done on-site since unstable and quickly decomposing to oxygen
  - ✓ Ozone generators using air or oxygen as source, with occasional oxygen concentrators
- when generated from air usual concentration 0.5-2% ozone
- with oxygen gas usual concentration 4 7% ozone

#### Use in effluent treatment

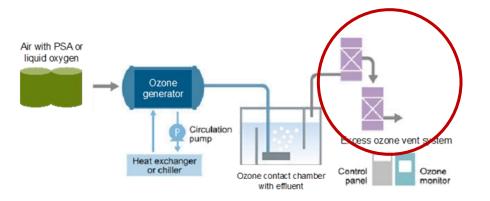
- Electrical discharge method most common source for generating ozone
  - ✓ Extremely dry air or pure oxygen exposed to controlled, uniform high-voltage discharge





#### Use in effluent treatment

- After generation, ozone fed into down-flow contact chamber containing wastewater to be treated
  - ✓ Aim to transfer ozone from gas bubble into bulk liquid with sufficient contact time for disinfection.
  - ✓ Commonly used contactor type diffused bubble
- co-current and counter-current
- variants: positive pressure injection, ventury, mechanically agitated and packed tower.



#### Use in effluent treatment

- Treatment of off-gases from to destroy any remaining ozone
  - ✓ In case of pure oxygen as feed-gas, recycling of off-gases from contact chamber possible to generate ozone or reuse in aeration tank.

#### Example



**Ozonator** (at Wylie Water Treatment Plant, North Texas)

### Ozone Treatment

- Little space required
- Destroy pathogens & organics
- Fast: less than 30 min
- No harmful residuals
- No bacteria regrowth
- Onsite generation of ozone
- Increase in dissolved oxygen

#### Ozone treatment Advantages



- High capital and operation & maintenance costs
- Need for highly skilled labor
- More complex than others
- Need for corrosion-resistant material (e.g. stainless steel)
- Not economical for removal of high levels of TSS/COD

Ozone treatment disadvantages

### Quality of tertiary treated effluent

- Quality of tertiary treated effluent depends on efficiency of basic effluent treatment, type of tertiary treatment & its management.
- Generally, the treated effluent after tertiary is nearly colourless, very low suspended solids and low level of organics.
- Still, the quality of this water may not conform to inlet requirements of membrane filtration such as Reverse Osmosis.
- Hence **pre-treatment to membranes** are required additionally for any recovery.

#### Table - Treated effluent quality Vs requirement for RO

Parameter	Unit	Effluent after tertiary	Required at inlet of RO
рН		6.5 – 7.5	6.5-7.0
Suspended solids	mg/l	5-15	<1
BOD/TOC	mg/l	5-10	<2
Total Nitrogen	mg/l	1-5	<5
Total hardness	mg/l	100-200	<250
Turbidity	NTU	10-20	<5
Calcium hardness	mg/l	75-150	<200
Silica	mg/l	15-20	<30
Oil & Grease	mg/l	0.3 -2	<1

### To remember



- While recovery & re-use of effluent seems attractive, it need high level of treatment efficiency in ETP.
- Presence of residual organics, fine suspended solids etc. need extensive pre-treatment for any recovery options.
- Membrane bio-reactors can be an effective modification to address these issues.
- Pressure filtrations are simple common tertiary treatment.
- Activated carbon treatment quite common in Bangladesh textile ETPs as polishing treatment
- Fenton treatment installed in few ETPs, preferred due to No sludge generation and low space requirement
- Advanced oxidation though costlier than other tertiary systems can remove residual organics

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