TRAINING PROGRAMME FOR ETP OPERATORS IN TEXTILE INDUSTRY

Promotion of Sustainability in the Textile and Garment Industry in Asia - FABRIC





Membrane-based treatment

GIZ FABRIC – ETP Operator Course



Contents



Use of nano-filtration

Use of membrane based bioreactors

Use of reverse osmosis

Aiming for zero-liquid discharge

Basic concept of membrane technology

Membranes

- fine filters capable to filter suspended and colloidal solids and sometimes dissolved solids.
- Performance depending on pore size of filters
- Common types of filters
 - Micron filters (MF)
 - Ultrafilters (UF)
 - Nano-filters (NF)
 - Reverse osmosis membranes (RO)

Types of filters

- Micron filters (MF)
 - for removing bacteria and viruses
 - generally used in membrane bio reactors (MBR)
- Ultrafilters (UF)
 - for removing all suspended and colloidal solids, turbidity and finelevel silt
 - commonly used in pre-treatment for reverse osmosis units

Types of filters

- Nano-filters (NF)
 - for removing organics
 - tighter NF also for multi-valent salts.
- Reverse osmosis membranes (RO)
 - for removing salts
 - used in most wastewater recycling systems and zero liquid discharge (ZLD) systems



Overview of filters by pore size





Types of membranes

- Plate and frame modules
- Tubular modules
- Spiral wound modules
- Hollow fiber modules



Types of membranes

- Plate and frame membranes
 - simplest configuration consisting of two end plates (flat sheet membrane spacers)
- Tubular modules
 - membrane inside of tube with feed solution pumped through

Types of membranes

- Spiral wound module
 - Most popular for nanofiltration or reverse osmosis membranes with flat sheet membrane wrapped around perforated permeate collection tube.
- Hollow fiber modules
 - used for seawater desalination
 - consisting of bundles of hollow fibers in pressure vessel
 - Often shell-side feed configuration with feed passing along outside of fibers and exiting at fiber ends.



Common applications for textile wastewater

- Membrane bio reactors using micro/ultrafilters for separation of biosolids
- Pre-treatment for RO systems with ultrafilter as part of water recycling/ZLD systems
- Nano-filtration segregation of salt solution from dye bath, enabling salt re-use in dyeing
- Reverse Osmosis as main component in water recycling / ZLD for removing salts from effluent.
- High pressure RO or membrane distillation for concentrating saline rejects from main RO unit



- Filtration of salt laden exhaust dye bath through nano-membrane:
 - salt allowed to pass
 - filtering out organics, colour and other impurities





- Pre-treatment of exhaust dye bath with 4 to 7% salt concentration
- Nanofiltration with clear salt solution and reject containing all colour and multivalent ions
- Decent recovery of salt solution without contamination with nano-filter of 400-500 Daltons (about 0.0008 microns)
- Control not easy!
- Mass balance of recovery process complicated
 - Recovered salt more than salt used (due to extra salt produced through reaction of acid/alkali in production)



Issues for consideration

- Only mono/divalent ions and water passing while hydrolized dyes and multivalent salts being retained.
- Theoretically possible to recover all salts; in practice recovery affected by various factors:
 - Large pore size (> 500 daltons) for good recovery of more than 70% of salt liquor, but passage of smaller organic molecules
 - recovered salt solution coloured and potentially unsafe for re-use
 - Narrow pore sizes (< 300 daltons) for good recovery of clear salt liquor safe for re-use but recovery rate low (less than 35%)
 - Presence of reacted salts





- MBR = Type of activated sludge treatment with micro or ultra filtration of biosolids instead of secondary settling tank
 - Higher MLSS in aeration tank possible (10000-15000 mg/l) since no limitations due to MLSS settling characteristics
 - Smaller size of units and less area required for ETP
- Development of submerged MBRs (with less power consumption) making MBR more popular
- Frequent fouling of membranes challenging
- External MBR (or side stream MBR) preferred system for small ETPs



Comparison of conventional activated sludge system and MBR



PUMPING STATION



Operation of MBR

Focus on

- Aerating in aeration tank
- Filtering effluent with set of micro/ultra filter
- Pumping back filtered MLSS into aeration tank



Operation of MBR

- Side stream MBR
 - Aeration tank contents pumped into external MBR mounted on skid.
- Submerged MBR
 - Ultrafilters stacked in cassettes and installed in aeration tank
 - Filtrate sucked out using vacuum or pressure pump



Operation of MBR

- Submerged membranes:
 - Airflow calculated with purpose of (a) aerating aeration tank and (b) continuously scouring and cleaning membrane surface.
- Back washing using air done to remove bio-solids sticking to membrane surface
- Side stream MBR cleaned with "clean-inprocess (CIP) using chemicals like caustic soda and acid



Variations of MBR

- Possible set-up of submerged MBR:
 - Membrane cassettes installed directly in aeration tank
 - aeration tank constructed with two compartments with membrane stack in one compartment
- Side stream MBR and air-lift MBR
 - Sidestream is external MBR, operates like a conventional UF.
 - In air-lift, scouring by air used as an additional backwash step. It is less common.



Submerged MBR with placement of membranes; photo: Courtesy Koch



Power consumption of different MBRs

- Submerged MBR:
 - 0.5 kWh/m³ of effluent treated.
 - Side stream MBR:
 - 2-4 kWh/m³ depending on the type of effluent.
- Side stream MBR with air lift:
 - 1 1.5 kWh/m³ depending on of type of effluent treated



Submerged MBR with placement of membranes; photo: Courtesy Koch



Comparison of MBR system set-ups



Return sludge

Operational aspects to consider

- Sludge retention time (SRT) in MBR high (30-50 days)
 - Solids filtered and retained in aeration tank
 - Higher SRT increasing chance of membrane fouling => membrane fouling reducing flow
- Two MBR operating modes
 - (1) Keeping constant pumping pressure with varying permeate flow
 - (2) Keeping constant permeate flow with varying pressure (better!)
- Better MBR performance at higher temperature (up to 450C)
 - Lower temperature increasing operating pressure due to higher viscosity

Common fouling control techniques

- 1. Membrane backwashing
- 2. Intermittent operation of submerged membranes
- 3. Air backwashing
- 4. Use of better membranes
- 5. Chemical cleaning



Common fouling control techniques

- 1. Membrane backwashing
 - permeate water pumped back to membrane
 - flows through pores to feed channel dislodging internal and external foulants

2. Intermittent operation of submerged membranes

- Stoppage of filtration at regular time intervals while continuing aeration
- Particles deposited on membrane surface dislodged in absence of suction



Common fouling control techniques

- 3. Air backwashing
 - pressurized air in membrane's permeate side building up and releasing significant pressure within very short period of time.

4. Use of better membranes

- Use of advanced anti-fouling membrane materials for ultrafiltration

Common fouling control techniques

- 5. Chemical cleaning
 - Daily chemically enhanced backwash
 - Weekly maintenance cleaning with higher chemical concentration
 - Intensive chemical cleaning (once or twice a year)

Advantages of MBR

- Better removal of BOD/COD and pathogens compared to conventional activated sludge systems
- Better degradation of complex organics/Oils & Grease due to higher sludge retention time
- Treated effluent very clear and less turbid
- Lesser pre-treatment when considering effluent recovery
- Good for ETPs with limited space and considering future recycling options

Disadvantages of MBR

- Higher capital cost for good system
- Higher operation and maintenance cost due to additional power and membrane cleaning/replacement
- System more sensitive and complex in operation
- Membrane replacement adding to list of consumables.





Process separating saline water from fresh water by membrane

- Membrane allowing passage of fresh water only
- pressure exerted by salt water called 'osmotic pressure'
- Reverse Osmosis (RO)
 - reversal of process by applying pressure on salt side to overcome osmotic pressure)
 - water from saline side passing to fresh water side





- Reverse Osmosis membranes finest pore size
 - Small enough to filter salt molecules and only allowing passage of water
- RO operating under very high pressure
 - pressure depending on salt concentration at system inlet
- Unlike MF or UF, in RO units no backwashing but only cleaning using chemicals



- RO system elements:
 - pre-treatment
 - high pressure pump
 - RO membranes stacked in a vessel
 - permeate collection





RO membranes

- Initially made of cellulose acetate
- Today mostly made of polyamide layer placed over poly sulfone layer and mounted on polyester base.
- Specialty coating on membranes to reduce membrane fouling



Spiral wound RO configuration

RO membranes

- Manufactured by modified polymerization process leaving openings in plastic (pore size)
- Different configuration depending on how membranes arranged in vessel
 - **Spiral wound** (most common)
 - Disc & tube or tubular



Spiral wound RO configuration

RO membranes – set-ups

Disc & tube (DT) RO configuration

- For DT membrane stack
 - RO membranes cut in hexagonal shape
 - placed on disk
 - process repeated to form cassette





- Need for extensive pre-treatment
 - Softening
 - needed to prevent fouling or scaling, if high hardness of treated effluent
 - use of zeolite softener, lime soda softener, pelletizer
 - Dosing of anti-scalants at RO to control scaling from calcium carbonate/sulfate
 - inlet kept at slightly acidic side



- Need for periodical membrane cleaning
 - RO recovery rate (flux rate) reducing due to scaling
 - cleaning-in-process (CIP) using special CIP chemicals with acid/alkali
 - Special membrane cleaning chemicals available
- Need for membrane replacement generally every 2
 4 years
 - Earlier when cleaning not improving recovery rate



Aiming for zero-liquid discharge (ZLD)

"No drop of water discharged"

- Objectives
 - to prevent wastewater discharge
 - To recover water for re-use
- Achieved in multiple stages



Steps involved

- Conventional physico-chemical and/or biological treatment for making effluent fit for RO
- 2. Pre-treatment processes removing hardness, silt, turbidity and organics to level preventing fouling of membranes
 - involving softening
 - pre-filtrations in MGF/ACF/ Micron filters



Steps involved

- Advanced oxidation methods to control organics
- Often inlet to RO protected with additional ultrafiltration membrane
- Multiple stage RO system to optimize recovery and minimize reject
 - initially, use of brackish water membranes
 - later stages, use of sea water membranes
- Evaporation of reject often after further concentration using high pressure RO system





Management of RO rejects

- Rejects about 8-15% of inlet volume
- Common approaches:
 - Purification with nano-filter and subsequent reuse of brine
 - Rejects of nano-filtration evaporated
 - Evaporation of entire reject and disposal of salts (since salt recovery not always feasible)
 - In cotton processing units feasible to recover sodium sulphate using adiabatic chiller and re-use in dyeing







Common issues with Denim effluent

Membranes affected by

- sizing agents (PVA or CMC and others)
- pumice stones residuals
- enzymes used in washing operations leading to chelating reactions with membrane materials
- indigo decreasing membrane flux and reducing output



Issues for consideration

- Always verify system performance promises by system suppliers
 - Often simpler designs (without membrane systems) using only tertiary oxidation and nano-level filtration.
- Need for high quality water in most textile operations, usually met by water recovered through membranes
- High cost of installation and operation & maintenance of ZLD
 - Initial investment Tk 1 1.5 Lakh per m³
 - O & M cost Tk 150 400 per m³ depending on need for and type of evaporation of RO reject (e.g. energy need, solar use)

Importance of good system design

- Proper and tailored system design for industrial use aiming for maximum recovery in RO and lowest quantity of saline reject
 - RO systems usually manufactured for saline, but clean water => risk of fouling
- Pre-requisites for good RO life (> 2 3 years) and decent recovery (>75%):
 - Iow COD
 - Iow hardness (particularly Calcium)
 - pre-treatments to reduce COD and hardness

Importance of good system design

- Control of turbidity in inlet water
 - pre-treatment of RO inlet using ultrafiltration to reduce Silt Density Index (SDI) to less than 5.
- Maximize recovery using three stage RO system
 - Membranes to be selected for each stage (brackish vs seawater, special coating to make it fouling resistant, high pressure etc.)

Advantages of ZLD

- Provision of full legal compliance with discharge standards as well as conformance to customer requirements
- Water security for industry facing critical water scenarios
- Better image with buyers, public, NGOs and authorities
- Important positive impact on protection of environment
- Water recovery ensuring zero loss of production
- Use of water from ZLD ensuring consistency and control in product quality



Disadvantages of ZLD

- Ensuring 100% 'zero' very difficult
- Costliest treatment in installation and prohibitively costly in operation affecting competitiveness of industry
- Disposal of evaporated mixed salt challenging.
- Need for adequate and ready technical support
- Need for trained staff for operation



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